APPLICATION OF GAS EXPANSION TO FLUID CIRCULATION DEVICES IN MANNED SPACE ASSEMBLIES

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This technical report has been reviewed and is approved.

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ABSTRACT

The power required to circulate fluids for various pressure drops and flow rates, and the power obtained from isentropic expansion of habitable gases for manned space assembly application have been investigated. The results demonstrate the feasibility of using habitable gases, stored under pressure, as potential energy sources to power fluid circulation devices. These findings indicate that significant weight savings can be obtained using the gas expansion technique to furnish the required power of fluid circulation as compared to using other power sources, such as batteries.
The aerospace engineer has recognized the necessity to minimize power, weight, and volume requirements of life supporting systems whenever possible since man's earliest conquests of space travel.

One particular problem area has been to reduce the associated weight of all components involved with circulating fluids in manned space assemblies. Although the amount of power required to circulate fluids is relatively low, the weight of associated power sources to furnish the power is quite high.

The purpose of this study is to determine the power required to circulate fluids for various pressure drops and flow rates and to determine the feasibility of employing gas expansion techniques to furnish the required power. The gases that are used to furnish habitable atmospheres within manned space assemblies can be considered to be potential power sources since in many instances these gases are stored at relatively high pressures. Gases, such as air and its components of oxygen and nitrogen, have been analyzed to determine the available power obtained in their expansion from storage pressure to the atmosphere pressure of the spacecraft.

SECTION II

POWER REQUIREMENTS FOR FLUID CIRCULATION

The power required to circulate fluids within manned space assemblies can be determined from Bernoulli's equation for incompressible fluid flow as given by the following expression:

\[
\frac{P_1}{\rho} + \frac{V_1^2}{2\rho} + gZ_1 + W = \frac{P_2}{\rho} + \frac{V_2^2}{2\rho} + gZ_2 + \frac{L}{\rho}
\]

where:

- \( \rho \) = density \(- \text{lbm/ft}^3\)
- \( P_1 \) = pressure upstream \(- \text{lbf/ft}^2\)
- \( P_2 \) = pressure downstream \(- \text{lbf/ft}^2\)
- \( V_1 \) = velocity upstream \(- \text{ft/sec}\)
- \( V_2 \) = velocity downstream \(- \text{ft/sec}\)
- \( Z_1 \) = position reference upstream \(- \text{ft}\)
Bernoulli's equation takes into account the amount of work required to change the potential energy, kinetic energy, and flow work of the fluid while overcoming friction losses. Equation 1 can be rewritten to determine the total pressure head which must be overcome by the circulation device to obtain the desired fluid flow characteristics.

\[ W_p = (P_2 - P_1) + (V_2 - V_1) \left( \frac{\rho}{2 \gamma} + (Z_a - Z_b) \right) + L \]  

(2)

where

\[ W_p = \text{Total Pressure Head} = H - \text{lbf/ft}^2 \]

The mass flow rate for fluid flow may be expressed by:

\[ G = \rho V A \quad \text{lbm/sec} \]  

(3)

where

\[ \rho = \text{density} \quad \text{lbm/ft}^3 \]
\[ V = \text{velocity} \quad \text{ft/sec} \]
\[ A = \text{cross sectional area} \quad \text{ft}^2 \]

The volumetric flow rate for fluid flow can be expressed by:

\[ Q = VA \quad \text{ft}^3/\text{sec} \]  

(4)

The mass flow rate and the volumetric flow rate can be expressed by combining equations 3 and 4 to obtain:

\[ G = QV \quad \text{lbm/sec} \]  

(5)

The power required to circulate fluids may be expressed by the following equation:

\[ P = \frac{W G}{C} \quad \text{hp} \]  

(6)
where
\[ C = 550 \frac{\text{lb} \cdot \text{ft}}{\text{sec} \cdot \text{hp}} \]

The power equation can also be expressed in terms of volumetric flow and total pressure head by combining equations 5 and 6 to yield the following:
\[ P = \frac{WqQ}{C} - \text{hp} \quad (7) \]
or
\[ P = \frac{HqQ}{C} - \text{hp} \quad (8) \]

The power equation can be rewritten, if \( H \) is expressed in inches of water (in. HgO) and \( Q \) is expressed in cubic feet per minute (cfm), to yield the following:
\[ P = 0.301575 (H)(Q) - \text{hp} \quad (9) \]

Equation 9 is expressed by figure 1 for various total pressure heads and flow rates. The power required to circulate fluids is a linear function of volumetric flow rate and the total pressure head created by the circulation device.

SECTION III
ISENTROPIC EXPANSION

The expansion of gas from a higher pressure to a lower pressure is the process which takes place when gases, such as oxygen, are released from their high storage supply to maintain habitable atmospheres within space assemblies. This process is assumed to occur so rapidly that no heat is transferred thereby classifying it as an adiabatic process. Also, it is assumed to be an ideal adiabatic process without friction losses to classify it as an isentropic process.

Bernoulli's equation for compressible fluid flow undergoing an isentropic process is given by the following expression:
\[ \Delta h_{\text{is}} = \frac{KRT}{k-1} \left[ \frac{P_a}{P_t} \right]^{\frac{k-1}{K}} - 1 \quad (10) \]

where:
\[ \Delta h_{\text{is}} = \text{the enthalpy change from condition 1 to 2 where upstream is 1 and downstream is 2} \]
\[ K = \text{the ratio of the specific heat of the gas at constant pressure to the specific heat at constant volume, or } \frac{C_p}{C_v} \]

\[ K_{\text{air}} = K_{O_2} = K_{N_2} = 1.4 \]

\[ R = \text{gas constant for the particular gas} \]

\[ R_{\text{air}} = 53.35 \frac{\text{ft-lbf}}{\text{lbm} \cdot \circ\text{R}} \]

\[ R_{O_2} = 48.29 \frac{\text{ft-lbf}}{\text{lbm} \cdot \circ\text{R}} \]

\[ R_{N_2} = 55.16 \frac{\text{ft-lbf}}{\text{lbm} \cdot \circ\text{R}} \]

\[ T_1 = \text{temperature upstream} \quad (\circ\text{R}) \]

\[ P_1 = \text{pressure upstream} \quad \frac{\text{lbf}}{\text{ft}^2} \]

\[ P_2 = \text{pressure downstream} \quad \frac{\text{lbf}}{\text{ft}^2} \]

This equation may be used to determine the enthalpy change encountered during compressible fluid flow from upstream conditions to downstream conditions. Graphs of this equation, using enthalpy change vs pressure ratio, are shown in figures 2, 3, and 4 for air, oxygen, and nitrogen, respectively. These graphs are obtained for the temperature range of 50° F to 100° F. The enthalpy change becomes asymptotic as the pressure ratio approaches rather large values.

**SECTION IV**

**AVAILABLE POWER FROM GAS EXPANSION**

The available power obtained from an isentropic gas expansion can be determined from the enthalpy change which occurs and the mass flow rate. The available power can be expressed by the following equation:

\[ P = (\Delta h_{1s})_G(C) \quad (11) \]

where

\[ P = \text{available power obtained from isentropic expansion} \quad \text{hp} \]

\[ \Delta h_{1s} = \text{the enthalpy change from condition 1 to 2 where upstream is 1 and downstream is 2} \quad \text{Btu/lbm} \]

\[ G = \text{mass flow rate} \quad \text{lbm/hr} \]

\[ C = \text{conversion constant} \quad \text{hp/2340 Btu} \]

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Graphs of equation 11 using available power vs pressure ratio for various mass flow rates at 80°F are shown in figures 5, 6, and 7. The temperature of 80°F was chosen because manned space assemblies are maintained at or near 80°F. This temperature choice will give a good approximation of available power vs pressure ratio between the temperature range from 50° to 100°F, since temperature does not greatly affect the enthalpy function between 50° and 100°F as shown in figures 2, 3, and 4. To derive the available power for a given pressure ratio at a temperature different from 80°F, yet between 50° and 100°F, use the available power data given in figures 5, 6, and 7 and multiply by \( \frac{T}{200} \). The temperature (T) must be expressed in degrees Rankine.

\textbf{SECTION V}

\textbf{CONCLUSIONS}

The major conclusion to be derived from this study is that available energy obtained from isentropic expansion of habitable gases can be used to furnish power for fluid circulation devices within manned space assemblies.

The engineer will have to take the friction losses and inefficiencies exhibited by real devices into account when he uses figure 1 and figures 5, 6, and 7 together to determine integrated systems. For instance, suppose two astronauts are maintained within a completely sealed spacecraft and they only require a total metabolic rate of 0.2 lbm/hr of oxygen. Figure 6 indicates that 60 x 10^-4 hp can be obtained for this flow rate at a pressure ratio of 10/1, or where P₁ is 200 psia and P₂ is 5 psia. If circulating devices integrated with impulse turbines are used, a total efficiency of 50% can be considered as a design factor. Thus, the real available power for the aforementioned pressure drop and mass flow rate would be approximately 30 x 10^-4 hp. This device could be used to circulate fluids within the manned space assembly for typical conditions of 30 cfm at a total head pressure of 2 in. H₂O or other similar condition, such as 2 cfm at a total head pressure of 10 in. H₂O as indicated by figure 1.

The savings to be realized when the weight of associated fluid circulation components and valving using the isentropic expansion technique as compared to the weight of associated fluid circulation components using other power sources, such as batteries, is considerably significant. The application of the gas expansion technique to fluid circulation devices in manned space assemblies should definitely be considered when the habitable gases are stored within vessels at pressures higher than the internal atmospheric pressure of the space assembly. This technique provides a method of using the energy which was transferred to the habitable gases, while being changed to high pressures on the earth, to be recovered and used during actual manned space travel.
Figure 1. Required Power vs Total Head for Fluid Flow
Figure 4. Enthalpy Change vs Pressure Ratio for Nitrogen
Figure 5. Available Power vs Pressure Ratio for Expansion Rates of Air at 80°F (T₁)
Figure 7. Available Power vs Pressure Ratio for Expansion Rates of Nitrogen at 80°F ($T_1$)
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